

Numerical Simulations of Wave Generation by a Vertical Plunger Using RANS and SPH Models

S. C. Yim, M.ASCE¹; D. Yuk²; A. Panizzo³; M. Di Risio⁴; and
P. L.-F. Liu, F.ASCE⁵

Abstract: The water wave generation by a freely falling rigid body is examined in this paper. Two different two-dimensional numerical approaches have been utilized to simulate the time histories of fluid motion, free surface deformation, and the vertical displacement of a rectangular-shape rigid body. While the first approach is based on the Reynolds-averaged Navier–Stokes (RANS) equations, with the k - ϵ closure model to compute the turbulence intensity, the second uses the smoothed particle hydrodynamics (SPH) method. Numerical simulations using several different initial elevations of the rigid body and different water depths have been performed. The displacement of the moving rigid body is determined by dynamic equilibrium of the forces acting on the body. Numerical results obtained from both approaches are discussed and compared with experimental data. Images of the free surface profile and falling rigid body recorded from the laboratory tests are compared with numerical results. Good agreement is observed. Numerical solutions for the velocity fields, pressure distributions, and turbulence intensities in the vicinity of the falling rigid body are also presented. The similarity and discrepancy between the solutions obtained by the two approaches are discussed.

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Introduction

Recently, significant progress has been made in the field of numerical analysis of fluid-structure interaction problems with the aid of advanced computing technology. Numerical tools for analyzing fluid flows and structural mechanics have been developed separately using different mathematical approaches. Conventionally, the Eulerian formulation is widely used to describe fluid flows, because it is relatively easy to implement the conservation laws of flow motions. On the other hand, the Lagrangian formulation has been a predominant approach in the development of numerical tools for structural mechanics because of the convenience in using the Lagrangian description for the material surface displacement and the dynamic response of the structural system. Recently, the mixed or arbitrary Eulerian–Lagrangian for-

mulation, which is necessary for coupling fluid and structural dynamic problems (Belytschko et al. 2000), has been used widely in developing a numerical model for fluid-structure interactions.

In studying fluid-structure interaction problems, it is essential to fully couple the motions of the structure and the ambient fluid flows. In an earlier study by Yuk et al. (2006), a numerical model has been developed, in which the coupling between the moving rigid body and fluid flows is based on an iterative procedure enforcing the principle of the dynamic equilibrium of the fluid, the structure, and their interfaces. In other words, the displacement of the structure and the fluid are determined in such a way that the dynamic equilibrium on the interface between fluid and rigid body is satisfied simultaneously at each time step. We note that the model presented by Yuk et al. (2006) is an extension of the Reynolds-averaged Navier–Stokes (RANS) model originally developed by Lin and Liu (1998a, b) for studying breaking waves in surf zone. A k - ϵ nonlinear eddy viscosity closure model was used in describing the statistical properties of turbulence. In Lin and Liu's model the volume of fluid (VOF) method is used to track the free surface locations. This model has been employed to investigate various problems concerning wave forces acting on stationary structures (e.g., Liu et al. 1999; Chang et al. 2001, 2005; Hsu et al. 2002; Liu and Al-Banaa 2004).

Smoothed particle hydrodynamics (SPH) is a numerical model based on a fully Lagrangian approach. SPH has been used in the last decade to model fluid flows considering the fluid as being made up of a finite number of particles, evolving in a mesh-free domain. Applications of SPH to modeling of landslide generated water waves have been successfully carried out by Monaghan and Kos (2000), Monaghan et al. (2003), Panizzo (2004a,b), and Panizzo and Dalrymple (2004).

In the present paper, the RANS model developed by Yuk et al. (2006) and the SPH model developed by Panizzo (2004a,b) are both applied to predict the aerial and submerged drop of a rigid

¹Professor, Ocean Engineering Program, Civil Engineering Dept., Oregon State Univ., Corvallis, OR 97331 (corresponding author). E-mail: solomon.yim@oregonstate.edu

²Staff Engineer, BSM Consulting Engineers, Inc., Astoria, OR 97103; formerly, Post Doctoral Student, Ocean Engineering Program, Civil Engineering Dept., Oregon State Univ., Corvallis, OR 97331.

³Post Doctoral Student, DISAT Dept., L'Aquila Univ., 67040 Montelucio di Roio, L'Aquila, Italy.

⁴Post Doctoral Student, Dept. of Civil Engineering, Tor Vergata Univ., Via del Politecnico 1, 00133 Rome, Italy.

⁵Professor, School of Civil and Environmental Engineering, Cornell Univ., Ithaca, NY 97331.

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68 body and the subsequent generation and propagation of waves. To
69 demonstrate their accuracy and capability, numerical results from
70 these models are compared with a set of experimental data. Spe-
71 cifically, the experiments involved dropping a weighted box ver-
72 tically into a body of water. The experimental study was carried
73 out in the framework of a research program on tsunami genera-
74 tion and propagation, performed at the LIAM laboratory of
75 L'Aquila University (Panizzo 2004a). In the present work, the
76 free surface deformation estimated from pictures taken during
77 the experiments and wave gauge data are used to validate and
78 compare the above mentioned numerical models.
79 The present paper is organized as follows: "Model Descrip-
80 tion" introduces the RANS and the SPH numerical models. Sub-
81 sequently, "Experimental Setup" describes the experimental setup
82 and program, while comparisons of model results and experimen-
83 tal data are discussed in "Numerical Results." Finally, summary
84 conclusions are presented in the "Concluding Remarks."

85 Models Description

86 For completeness, both the RANS equations model and the SPH
87 model are briefly described here. More details can be found in Lin
88 (1998), Panizzo (2004a,b), and Yuk et al. (2006).

89 RANS Model

90 As shown in Lin and Liu (1998a) the ensemble averaged mean
91 flow field is solved by using RANS equations that are given as

$$\frac{\partial \langle u_i \rangle}{\partial x_i} = 0 \quad (1)$$

$$\frac{\partial \langle u_i \rangle}{\partial t} + \langle u_j \rangle \frac{\partial \langle u_i \rangle}{\partial x_j} = -\frac{1}{\langle \rho \rangle} \frac{\partial \langle p \rangle}{\partial x_i} + g_i + \frac{1}{\langle \rho \rangle} \frac{\partial \langle \tau_{ij}^m \rangle}{\partial x_j} - \frac{\partial \langle u'_i u'_j \rangle}{\partial x_j} \quad (2)$$

94 where subscripts i and j ($=1, 2$) denote Cartesian components for
95 two-dimensional flows and $\langle \rangle$ =ensemble average of the physical
96 variables appearing in the Navier–Stokes (NS) equations. In Eqs.
97 (1) and (2), u_i denotes i th component of the velocity vector;
98 ρ =density of fluid; p =pressure; g_i = i th component of the gravi-
99 tational acceleration; and τ_{ij}^m =molecular viscous stress tensor. For
100 a Newtonian fluid, τ_{ij}^m can be expressed by $\tau_{ij}^m = 2\mu\sigma_{ij}^m$ with μ
101 being dynamic viscosity and $\sigma_{ij} = (\partial u_i / \partial x_j + \partial u_j / \partial x_i) / 2$ strain rate
102 tensor. In Eq. (2), the Reynolds stress tensor is defined as

$$R_{ij} = -\langle \rho \rangle \langle u'_i u'_j \rangle \quad (3)$$

104 In previous research work, many second-order turbulence closure
105 models have been developed for different applications. In this
106 paper, the k - ϵ model, where the Reynolds stress is approximated
107 by a nonlinear algebraic stress model, is employed for turbulence
108 closure (Lin and Liu 1998a; Shih et al. 1996).

$$\rho \langle u'_i u'_j \rangle = \frac{2}{3} \rho k \delta_{ij} - C_d \frac{k^2}{\epsilon} \left(\frac{\partial \langle u_i \rangle}{\partial x_j} + \frac{\partial \langle u_j \rangle}{\partial x_i} \right) + \left[C_1 \left(\frac{\partial \langle u_i \rangle}{\partial x_l} \frac{\partial \langle u_l \rangle}{\partial x_j} + \frac{\partial \langle u_j \rangle}{\partial x_l} \frac{\partial \langle u_l \rangle}{\partial x_i} - \frac{2}{3} \frac{\partial \langle u_l \rangle}{\partial x_k} \frac{\partial \langle u_k \rangle}{\partial x_l} \delta_{ij} \right) - \frac{\rho k^3}{\epsilon^2} + C_2 \left(\frac{\partial \langle u_i \rangle}{\partial x_k} \frac{\partial \langle u_j \rangle}{\partial x_k} - \frac{1}{3} \frac{\partial \langle u_l \rangle}{\partial x_k} \frac{\partial \langle u_l \rangle}{\partial x_k} \delta_{ij} \right) + C_3 \left(\frac{\partial \langle u_k \rangle}{\partial x_i} \frac{\partial \langle u_k \rangle}{\partial x_j} - \frac{1}{3} \frac{\partial \langle u_l \rangle}{\partial x_k} \frac{\partial \langle u_l \rangle}{\partial x_k} \delta_{ij} \right) \right] \quad (4)$$

111 where C_1 , C_2 , and C_3 =empirical coefficients; δ_{ij} =Kronecker

delta; $k = \frac{1}{2} \langle u'_i u'_i \rangle$ =turbulence kinetic energy; and $\epsilon = \nu \langle (\partial u'_i / \partial x_k)^2 \rangle$ =dissipation rate of turbulence kinetic energy with
 $\nu = \mu / \rho$ =kinematic viscosity. Eq. (4) returns to classical linear
isotropic eddy viscosity model when $C_1 = C_2 = C_3 = 0$ as shown
below

$$\langle u'_i u'_j \rangle = -2\nu_t \langle \sigma_{ij} \rangle + \frac{2}{3} k \delta_{ij} \quad (5)$$

where $\nu_t = C_d (k^2 / \epsilon)$ =eddy viscosity; and C_d =another empirical
coefficient. The turbulence closure model given in Eq. (4) can be
applied to general anisotropic turbulent flows. The governing
equation for k and ϵ (Rodi 1980) are modeled as

$$\frac{\partial k}{\partial t} + \langle u_j \rangle \frac{\partial k}{\partial x_j} = \frac{\partial}{\partial x_j} \left[\left(\frac{\nu_t}{\sigma_k} + \nu \right) \frac{\partial k}{\partial x_j} \right] - \langle u'_i u'_j \rangle \frac{\partial \langle u_i \rangle}{\partial x_j} - \epsilon \quad (6)$$

$$\frac{\partial \epsilon}{\partial t} + \langle u_j \rangle \frac{\partial \epsilon}{\partial x_j} = \frac{\partial}{\partial x_j} \left[\left(\frac{\nu_t}{\sigma_\epsilon} + \nu \right) \frac{\partial \epsilon}{\partial x_j} \right] + C_{1\epsilon} \frac{\epsilon}{k} \nu_t \left(\frac{\partial \langle u_i \rangle}{\partial x_j} + \frac{\partial \langle u_j \rangle}{\partial x_i} \right) \frac{\partial \langle u_i \rangle}{\partial x_j} - C_{2\epsilon} \frac{\epsilon^2}{k} \quad (7)$$

where σ_k , σ_ϵ , $C_{1\epsilon}$, and $C_{2\epsilon}$ =empirical coefficients. The coeffi-
cients in Eqs. (4)–(7) have been determined by performing many
simple experiments and enforcing the physical realizability
condition; the values for these coefficients employed by Lin and
Liu (1998a): $C_1 = 0.0054$, $C_2 = -0.0171$, $C_3 = 0.0027$, $C_d = 1.44$,
 $C_{2\epsilon} = 1.9$, $\sigma_\epsilon = 1.3$, and $\sigma_k = 1.0$, are also used in this study.

Applying appropriate boundary conditions, and approximating
the derivatives in the Navier–Stokes equations using a finite-
difference scheme with a combination of backward and forward
difference methods, numerical solutions are obtained. Detailed
descriptions of the numerical algorithms, such as the two-step
projection method for solving RANS equations (Chorin 1968)
and the VOF method for tracking free surface locations (Hirt and
Nichols 1981) as well as boundary conditions can be found in a
previous study by Lin and Liu (1998a).

SPH Model

SPH is a particle Lagrangian numerical model, which was first
introduced in astrophysics by Lucy (1977) and Gingold and Mon-
aghan (1977), and then adapted by Monaghan (1994) to simulate
free surface fluid flows. The model is based on two fundamental
ideas that every flow characteristic is smoothed over the spatial
domain by using an appropriate kernel function W , and that the
smoothed flow is approximated by particles, whose time evolu-
tion is governed by a Lagrangian scheme. There are no con-
straints imposed on the geometry of the system or on how far it
may evolve from the initial conditions. The equations of fluid
dynamics are transformed into integral equations by using the
kernel function W , which presents a finite interaction radius equal
to $2h$. The kernel is indeed a weighting function that smoothes out
field contributions defining the value of a physical variable, say A ,
at a certain point \mathbf{r} . In this approach, the kernel estimate of A is
defined as (Morris 1996)

$$A(\mathbf{r}) = \int_{\text{space}} A(\mathbf{r}') W(\mathbf{r} - \mathbf{r}', h) d\mathbf{r}' \quad (8)$$

The kernel function W has to satisfy the following two constraints

$$\int_{\text{space}} W(\mathbf{r}-\mathbf{r}',h)d\mathbf{r}'=1 \quad \text{and} \quad \lim_{h \rightarrow 0} W(\mathbf{r}-\mathbf{r}',h)=\delta(\mathbf{r}-\mathbf{r}') \quad (9)$$

In other words, W =smoothing function with a compact support, approximating a Dirac delta function. In the same manner, it is possible to estimate the gradient of a given function as (Morris 1996; Schlatter 1999)

$$\nabla_{\mathbf{r}}A(\mathbf{r})=\int_{\text{space}} A(\mathbf{r}')\nabla_{\mathbf{r}}W(\mathbf{r}-\mathbf{r}',h)d\mathbf{r}' \quad (10)$$

In the SPH numerical implementation, the fluid domain is represented by a certain finite number of particles, carrying the physical variable at the points occupied by their volumes. Starting from Eqs. (8) and (10), if we refer to a finite number of particles in a finite domain, under the hypothesis that the kernel, the variable, or both go to zero at infinity, it is possible to write the SPH estimation of the physical variable A and its gradient as a summation over neighbors b of particle a , such as

$$A_a=\sum_{b=1}^N V_b A_b W_{ab}, \quad \text{and} \quad \nabla_a A_a=\sum_{b=1}^N V_b A_b \nabla_a W_{ab} \quad (11)$$

where $W_{ab}=W(\mathbf{r}_a-\mathbf{r}_b,h)$; $V_i=m_i/\rho_i$; and ∇_i implies spatial derivative with respect to coordinates of the generic particle i .

It can be demonstrated (Morris 1996; Schlatter 1999) that the gradient of the physical variable A at hand can be rewritten as

$$\nabla_a A_a=\frac{1}{\rho_a} \sum_{b=1}^N m_b (A_b - A_a) \nabla_a W_{ab} \quad (12)$$

Using this approximation process, it is possible to rewrite the continuity equation as

$$\frac{d\rho_a}{dt}=\sum_{b=1}^N m_b (\mathbf{v}_a - \mathbf{v}_b) \nabla_a W_{ab} \quad (13)$$

The momentum equation for an inviscid and compressible fluid (Euler equation) reads

$$\frac{d\mathbf{v}_a}{dt}=-\sum_{b=1}^N m_b \left(\frac{P_b}{\rho_b^2} - \frac{P_a}{\rho_a^2} \right) \nabla_a W_{ab} \quad (14)$$

In the present work we take into account a real fluid by rewriting Eq. (14) as suggested by Monaghan (1994), as

$$\frac{d\mathbf{v}_a}{dt}=-\sum_{b=1}^N m_b \left(\frac{P_b}{\rho_b^2} - \frac{P_a}{\rho_a^2} + \Pi_{ab} \right) \nabla_a W_{ab} \quad (15)$$

where Π_{ab} =artificial viscous pressure and it is defined as

$$\Pi_{ab}=\begin{cases} \frac{-\alpha c_{ab} \mu_{ab} + \beta \mu_{ab}^2}{\rho_{ab}} & \text{if } \mathbf{v}_{ab} \cdot \mathbf{r}_{ab} < 0 \\ 0 & \text{otherwise} \end{cases} \quad (16)$$

with $\mu_{ab}=h\mathbf{v}_{ab} \cdot \mathbf{r}_{ab}(\mathbf{r}_{ab}^2+\eta^2)$; $\rho_{ab}=(\rho_a+\rho_b)/2$; $c_{ab}=(c_a+c_b)/2$; c_a and c_b =speed of sound evaluated at particles a and b positions; h =smoothing length; $\eta^2=0.01h$; and α and β =constants usually assuming values $\alpha=0.01$; $\beta=0.0$ for general hydraulic problems.

In this paper the kernel function proposed by Johnson et al. (1996) is employed, because it is well suited to simulate impacts between rigid bodies and the water. It is defined in the range $s=r/h \in [0.0; 2.0]$, as

$$W(\mathbf{r},h)=\frac{1}{\pi h^2} \left(\frac{3}{8}s^2 - \frac{3}{2}s + \frac{3}{2} \right) \quad (18)$$

$$W'(\mathbf{r},h)=\frac{1}{\pi h^3} \left(\frac{3}{4}s - \frac{3}{2} \right) \quad (17)$$

A state equation, defined as $p=B[(\rho/\rho_0)^\gamma-1]$, with $\gamma=7.0$ and $\rho_0=1,000.0 \text{ kg/m}^3$, is used in the model to relate density and pressure.

Experimental Setup

A series of experiments for water wave generation by a solid body plunger (Scott Russell wave generator) has been conducted at LIAM laboratory, L'Aquila University, Italy (Di Risio 2005). The experiments were performed in a three-dimensional flume 12 m long, 0.45 m deep, and 0.3 m wide (see Fig. 1). Rectangular cylinders with width=0.3 m (same as flume), height=0.1 m (vertical direction), and variable length (in flume direction, see Table 1 and Fig. 1) are released vertically at one end of the flume to generate waves. The space between the cylinder and the vertical walls of the flume is less than 1 mm. The specific weight of the cylinder is 1.33 t/m³. Three lengths of rectangular rigid body (0.05, 0.1, and 0.15 m) are used. Twenty one tests were conducted (see Table 1). Three different initial elevations of the cylinder are tested: partially submerged (the bottom of the cylinder is 3 cm below the still water level); on the still water level; and aerial (3 cm above the still water level). The water depth in the flume is also varied: 6, 10, 18, and 23 cm. Among these tests, three representative cases (L10H10M3, L10H10P3, and L10H18P3) are discussed in this paper.

During the experiments, five wave gauges are installed along the flume to measure the free surface elevation. A digital video camera (Canon XM1) with a frame acquisition rate of 25 Hz is used to record the wave profile in the generation region.

Numerical Results

The free falling rectangular body and the subsequent wave generation and propagation are modeled in the two-dimensional (2D) vertical plane. For the RANS model, a computational domain of 1.4 m \times 0.4 m is discretized with uniform grid size of 0.5 cm in horizontal direction and 0.25 cm in vertical direction. A rectangular shape rigid body is placed at the left end of the domain at a given height relative to the still water free-surface level and allows falling under gravity. Free-slip boundary conditions are applied on all the boundaries except at the right end of the computational domain, where the radiation boundary condition is imposed so as to ensure outgoing waves through the boundary. The same k - ϵ model is used for the boundary layer on the solid boundary including a vertical plunger.

In the numerical simulations, it is assumed that there is no space between the rigid boundary of the falling cylinder and the left boundary of the computational domain and the motion of falling body is always in perfectly vertical direction without rotation. The frictional forces acting on the surfaces of the box that are in contact with the vertical wall of the flume are assumed to be proportional to the contact area of the body with the wall, i.e., larger frictional forces are used for the box with larger dimension. The dynamic coefficient of friction used for the computation of three representative cases is $\mu=0.66$.

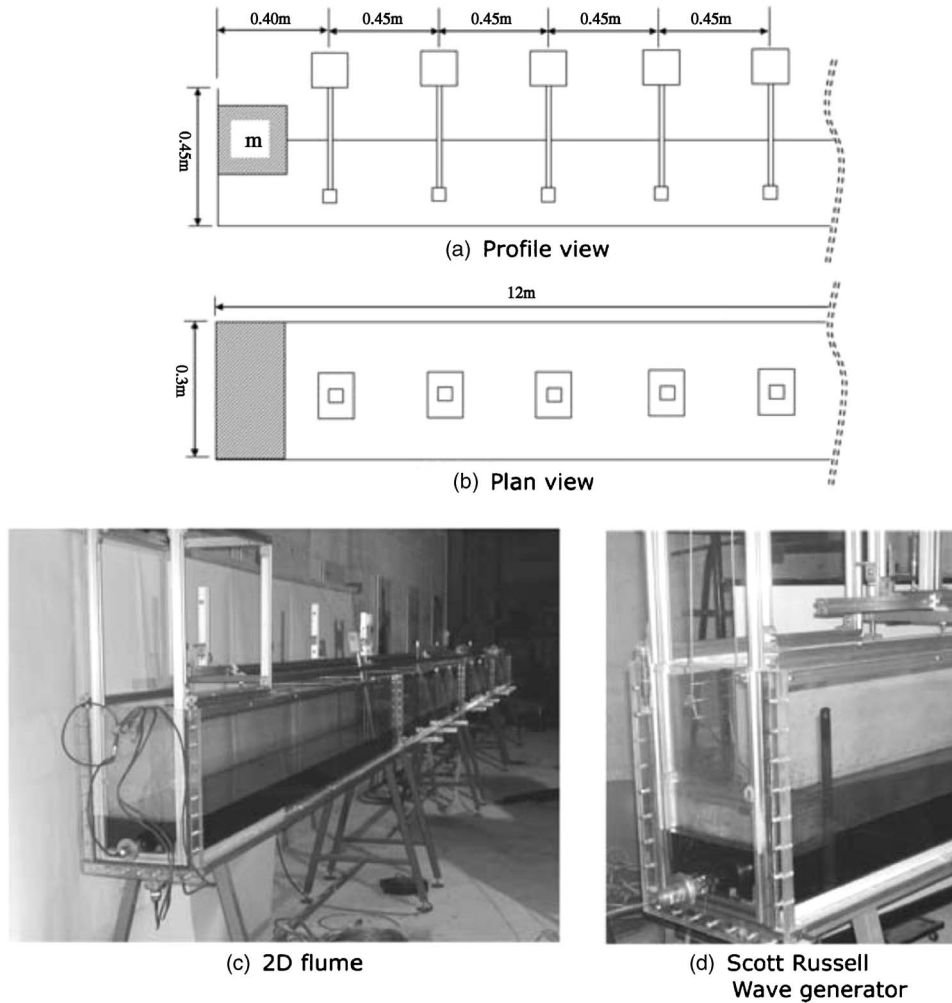


Fig. 1. (a), (b) Locations of wave gauges; (c) picture of 2D flume; and (d) Scott Russell wave generator

251 In computing the total force on the falling cylinder, the shear
 252 stress induced by flow motions, which is applied in a tangential
 253 direction on the moving boundary, is assumed to be negligible.
 254 Thus, only the normal forces obtained by integrating pressures
 255 along the moving boundaries are considered in this study. Motion
 256 of the cylinder for the RANS model is advanced by solving dy-
 257 namic equilibrium. The validity of the shear force assumption will
 258 be examined in a later section and further discussed in the “Con-
 259 cluding Remarks.”

260 For the SPH model, numerical simulations have been carried
 261 out using a computational domain of $2.0 \text{ m} \times 0.5 \text{ m}$, with particle
 262 diameter equal to 0.004 m . Initially, particles have been placed on
 263 a regular grid, with uniform grid size of 0.004 m . Boundaries and
 264 the rigid box falling into water have been modeled using repellent
 265 particles (Monaghan 1994), with free-slip conditions on all sur-
 266 faces. In all simulations, the α parameter assumed the value
 267 $\alpha=0.07$. Motion of the cylinder for the SPH model is prescribed
 268 by the experimental data. No dynamic equilibrium is considered.

269 For both RANS and SPH models, mesh regeneration is not
 270 required during the simulation. The same rectangular mesh in
 271 Cartesian coordinate is used with moving boundary condition
 272 throughout the simulation.

273 Three-dimensional effects are observed in some of the experi-
 274 ments. Differences in the free-surface elevation on one side wall
 275 of tank and the other side wall were noticed. However, these 3D

effects occurred when the wave was propagating after the wave 276
 generation. It is noted that 3D effects are negligible in the wave 277
 generation region. 278

For the numerical simulations and comparisons presented in 279
 the following sections, the Reynolds numbers ranges from $2.3e$ 280
 $+4$ to $5.9e+4$, the Froude number from 0.22 to 0.42, and simu- 281
 lation step sizes range from 0.0005 to 0.005, respectively. 282

Comparisons of RANS and SPH Model Predictions 283

284 Three selected cases of the physical experiments are presented in
 this section to examine the prediction capabilities between the 285
 two numerical models. The same rigid body is employed in all 286
 three cases. However, Cases I and II have identical water depths 287
 but different initial rigid body vertical locations. In Case I, the 288
 bottom of the rigid body is initially below the still water level 289
 (SWL) whereas in Case II, the bottom of the body is above the 290
 SWL. For Case III, the bottom of the rigid body has identical 291
 initial height with respect to the SWL as in Case II. However, the 292
 body is dropped into a large water depth. 293

Case I 294

In the first representative case (referred to as Test L10H10M3), 295
 the rigid body with dimensions of $0.1 \text{ m} \times 0.3 \text{ m} \times 0.1 \text{ m}$ 296
 (length \times width \times height) is located initially 3 cm below the SWL 297

Table 1. Experiments Configurations

Initial box location (cm)	Box length (cm)	Water depth (cm)	Test
+3	5	6	L5H6P3
		10	L5H10P3
	10	6	L10H6P3
		10	L10H10P3
		18	L10H18P3
		23	L10H23P3
-3	5	6	L5H6M3
		10	L10H6M3
	10	10	L10H10M3
		18	L10H18M3
		23	L10H23M3
		6	L15H6M3
0	5	6	L5H6PM0
		10	L5H10PM0
	10	18	L5H18PM0
		6	L10H6PM0
		10	L10H10PM0
		18	L10H18PM0
15	6	L15H6PM0	

and is released into the 0.1 m deep water. The time history of box displacement computed based on the RANS model is compared with experimental data in Fig. 2. Very good agreement is observed. We remark here that the numerically simulated displacement of the falling rigid body does not reach the bottom of the flume. In both SPH and RANS, simulation of the rigid body motion based on dynamic equilibrium is stopped when the bottom of the rigid body reaches a distance less than the particle diameter, in the case of SPH, and the last computational cell height, in the case of RANS, above the bottom of the flume to avoid numerical instability. After this time step, consistent with the physics of the experiment, the rigid body is held in place while simulation of the fluid dynamic continues. This procedure is applied to simulations

for all cases examined in this paper. The numerical instability and the limitation of the model will be further discussed later in this paper.

A snapshot of the free surface profile and the location of the cylinder at $t=0.32$ s is also shown in Fig. 2. The numerical (RANS) solutions for the locations of boundaries of the rigid body and the free surfaces are shown in thick solid lines, which are overlapped on the experimental image for direct comparisons. Again, very good agreement with experimental data is observed.

The time series of the free surface elevation at $x=0.4$ and 0.85 m of Test L10H10M3 for both RANS and SPH numerical predictions are shown together with the measured experimental data in Fig. 3. The generated wave is a solitary-like wave with small trailing waves. Both numerical predictions match the experimental results well, with the SPH model being slightly more dissipative, resulting in a less oscillatory motion of the free surface after the main wave has passed. The calculated maximum wave heights at both stations show good agreement with experimental data. However, a slight phase difference is observed, which could be caused by the different reference times used in the experiment measurements.

Figs. 4 and 5 show the predicted pressure and velocity fields, respectively, of the RANS and SPH models at various times. While the rigid body is falling, high pressures are observed at the bottom left corner of the flume, where the velocity is diminishing, and at the same time flow separation occurs at the bottom right corner of the moving body as shown in the snapshots at $t=0.2$ s of Figs. 4 and 5. Subsequently, a large counterclockwise vortex is generated in the front of the moving body (see Fig. 5). The RANS model results show that the vortex is advected downstream (positive x direction) with a much slower speed than the phase speed of the generated solitary-like wave. Furthermore, the SPH results indicate that the vortex is attached to the front face of the rigid body until the body reaches the bottom of the flume. This discrepancy in two numerical results needs to be further examined with velocity measurements. We also observe that the pressure near the vortex center is less than the hydrostatic pressure.

Case II

In the second case (Test L10H10P3), the rigid body size and water depth are the same as those in Case I. However, the initial elevation of the bottom of the cylinder is 3 cm above the SWL.

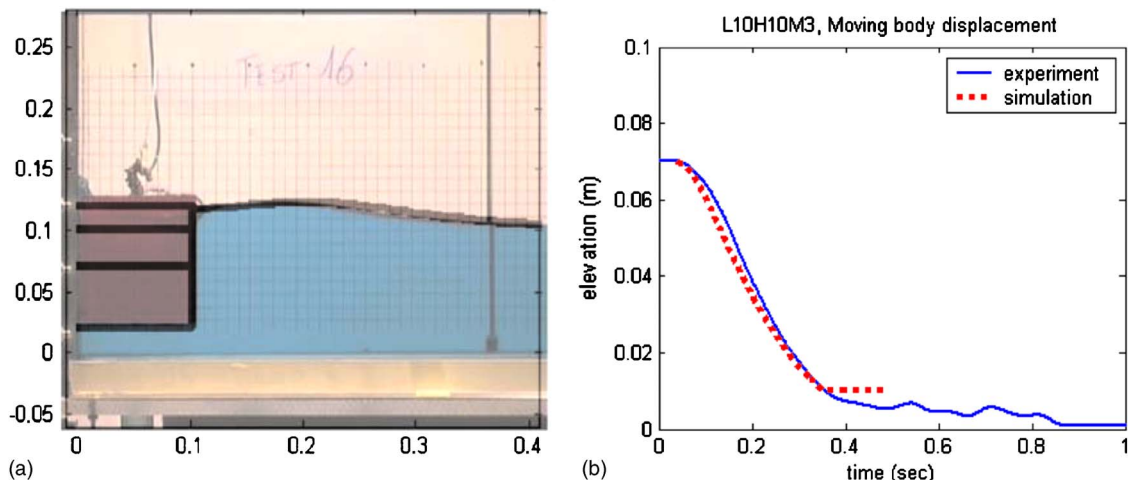


Fig. 2. Snapshot of rigid body with free surface profile at $t=0.32$ s (a); time history of rigid body displacement (b) (Case I, Test L10H10M3)

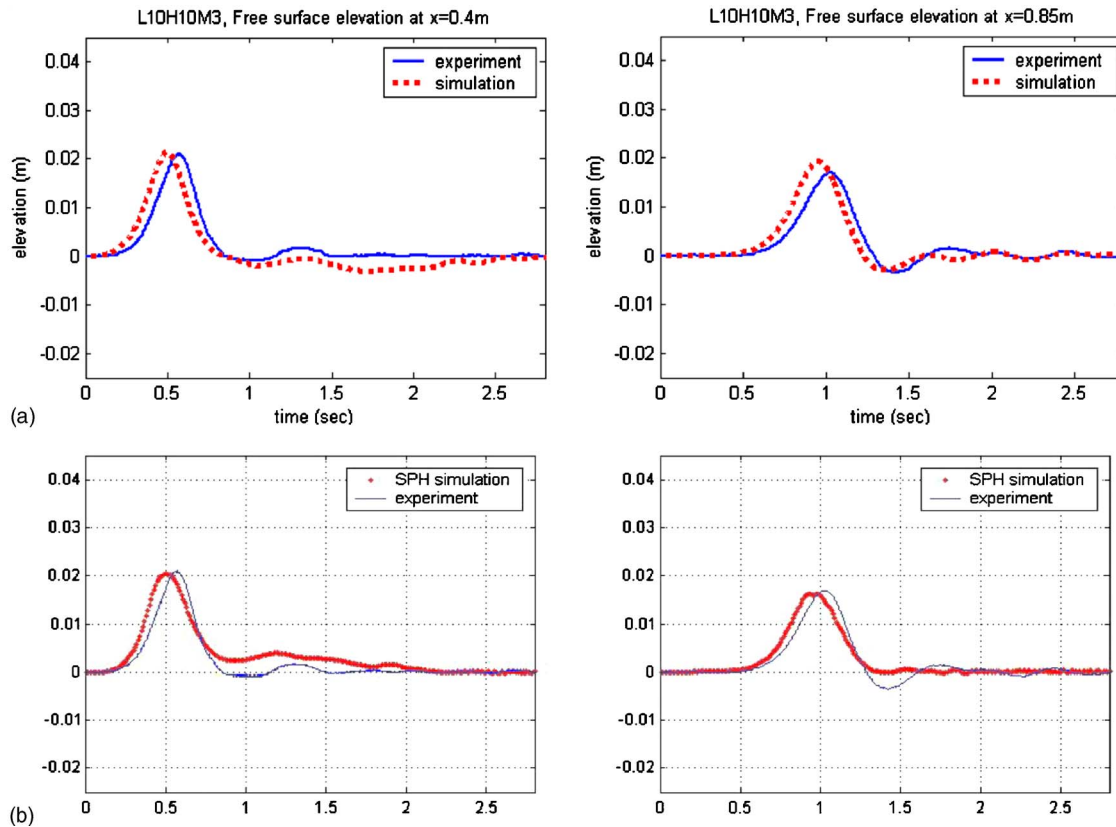


Fig. 3. Time histories of free surface elevation at $x=0.4$ and 0.85 m obtained from RANS model (a); SPH model (b) (Case I, Test L10H10M3)

352 The numerical results and experimental data for the movement of
 353 the falling cylinder and the snapshot of the free surface profile at
 354 $t=0.32$ s are shown in Fig. 6. Since the initial elevation of the
 355 cylinder is above the SWL, as the cylinder impacts and enters the
 356 water body, violent flow motions and free surface splashing occur.
 357 As shown in Fig. 6, the RANS model predicts the free surface
 358 reasonably well except that the splash height is underpredicted,
 359 which could be caused by the lack of required grid resolution in
 360 the numerical model. The time histories of free surface displacement
 361 at $x=0.4$ and 0.85 m are plotted in Fig. 7. It is clear that
 362 because the initial potential energy of this case is larger than that
 363 of the previous case, larger waves (the wave height to water depth
 364 ratio is about 0.4 at $x=0.4$ m) are generated near the plunging
 365 cylinder and the leading wave attenuates significantly between
 366 these two wave gauge locations (the wave height to water depth
 367 ratio is reduced to 0.3 at $x=0.85$ m). Furthermore, the amplitude
 368 dispersion seems to play an important role since the width of the
 369 leading wave has increased. The numerical results obtained from
 370 both the RANS and SPH models show slightly faster propagation
 371 speeds. As shown in Figs. 8 and 9, the influence of the falling
 372 rigid body on the fluid motion is much stronger than in the pre-
 373 vious case with an initially submerged location. The free surface
 374 in the front face of the moving body is separated during the im-
 375 pact and higher pressures near the bottom left corner of the flume
 376 are observed as in the previous case.

377 Case III

378 In the third case (Test L10H18P3), the same size of cylinder is
 379 initially located 3 cm above the SWL and released into 0.18 m
 380 deep water, which is deeper than that in the previous two cases.
 381 The snapshot in Fig. 10 shows the position of falling rigid body
 382 and the free surface profile generated at $t=0.32$ s. The numerical

results are in reasonably good agreement with the experimental 383
 data. Up to the point when the top of the falling rigid body is at 384
 the SWL, the pressure and velocity fields show behavior similar 385
 to those in Case II (Figs. 12 and 13). However, since the water 386
 depth is larger than the height of the falling cylinder, as the cyl- 387
 nder moves farther downwards (i.e., the top of cylinder becomes 388
 below the SWL) it is overtopped by a wave propagating towards 389
 the left end of the flume, which is then reflected back into the 390
 flume. Splashing at the end wall with strong turbulence intensity 391
 is observed (see Figs. 12 and 13). Unlike in the previous two 392
 cases, the vortex generated in front of the falling cylinder remains 393
 attached throughout the entire process. Discrepancy between numer- 394
 ical results and the experiment data are noticeable in compar- 395
 isons of the time histories of free surface elevation after $t \approx 1.5$ s 396
 (see Fig. 11). While the amplitude and phase of the leading wave 397
 is predicted accurately by both models, the RANS model results 398
 show a significant phase lag at the location $x=0.4$ m. On the other 399
 hand, the SPH model does not predict well the amplitude of the 400
 third and higher trailing waves at the location $x=0.4$ m and the 401
 shape of the second and higher trailing waves at the location x 402
 $=0.85$ m. We remark here that the random nature of the splashing 403
 fluid particles and 3D air bubbles observed in the experiments 404
 might cause these discrepancies. 405

406 Turbulence Intensity

A study of the turbulence behaviors induced by different falling 407
 heights and bodies (i.e., Cases I–III) is presented in this section. 408
 Only results from RANS model predictions are examined here 409
 because turbulence intensity predictions from direction SPH com- 410
 putation and measured turbulence data are not available. 411

Fig. 14(a) shows the time evolution of the turbulence intensity 412

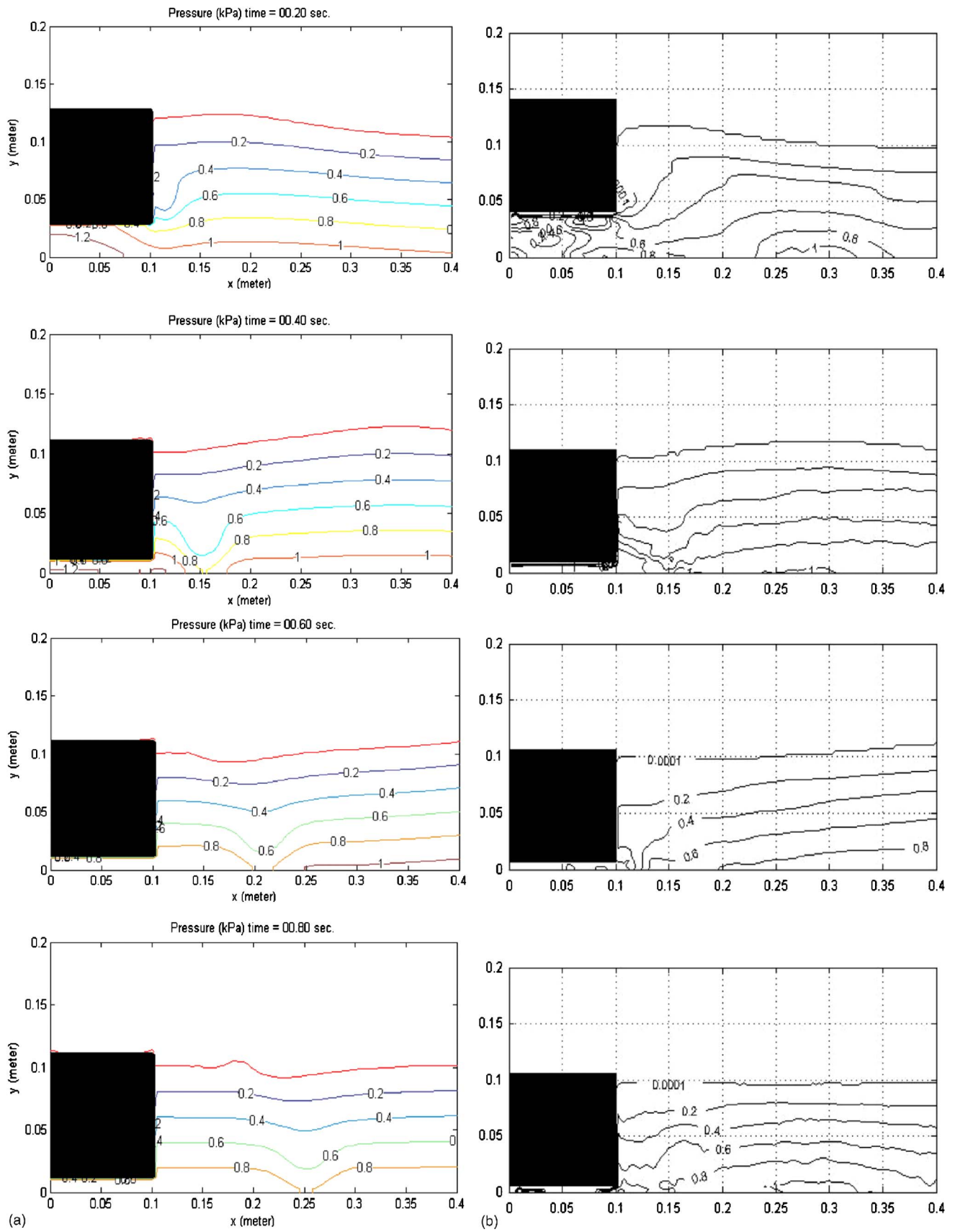


Fig. 4. Contour plots of pressure field computed by RANS (a); SPH (b) models at $t=0.2, 0.4, 0.6,$ and 0.8 s (Case I, Test L10H10M3)

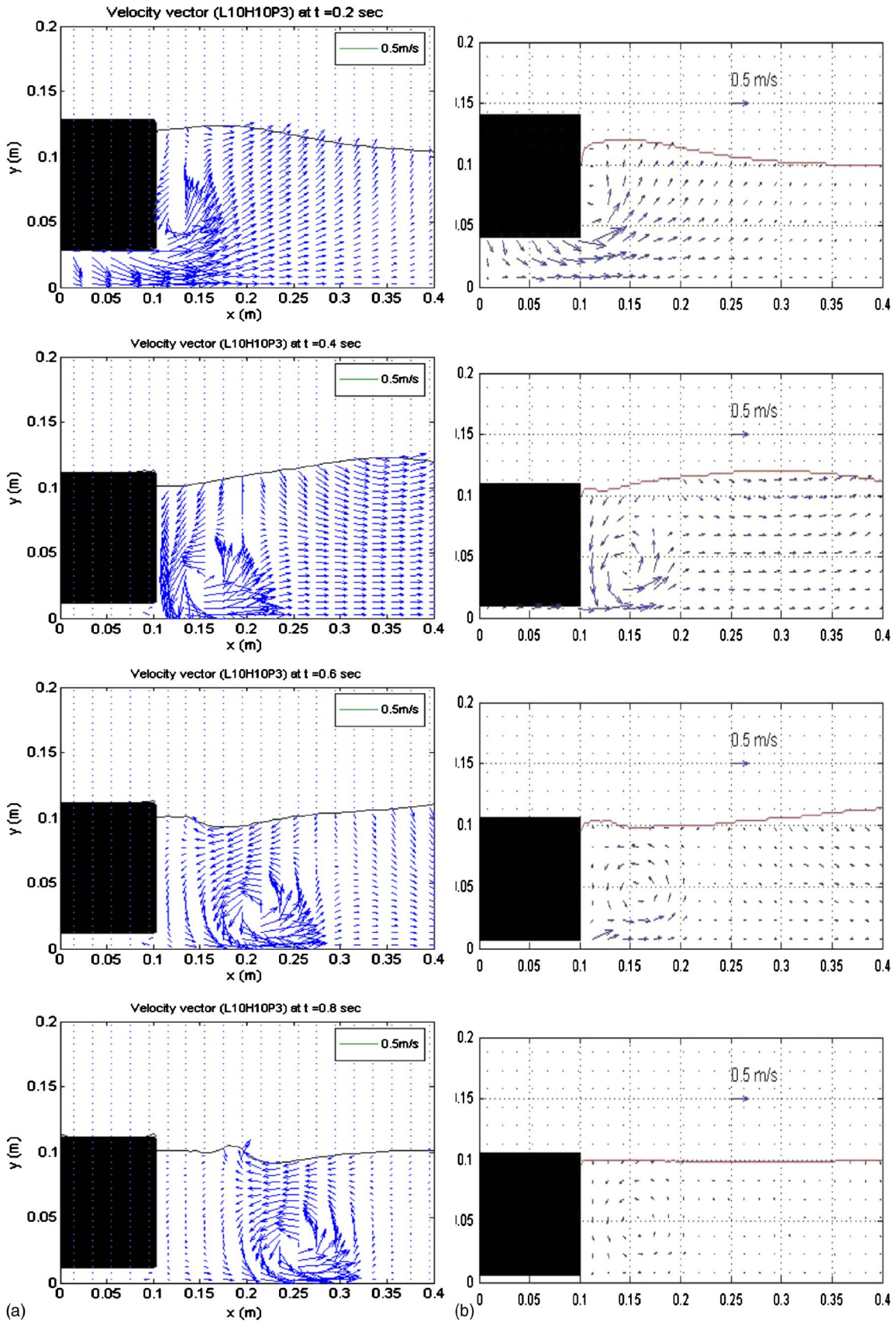


Fig. 5. Vector plots of velocity field computed by RANS model (a); SPH model (b) at $t=0.2, 0.4, 0.6,$ and 0.8 s (Case I, Test L10H10M3)

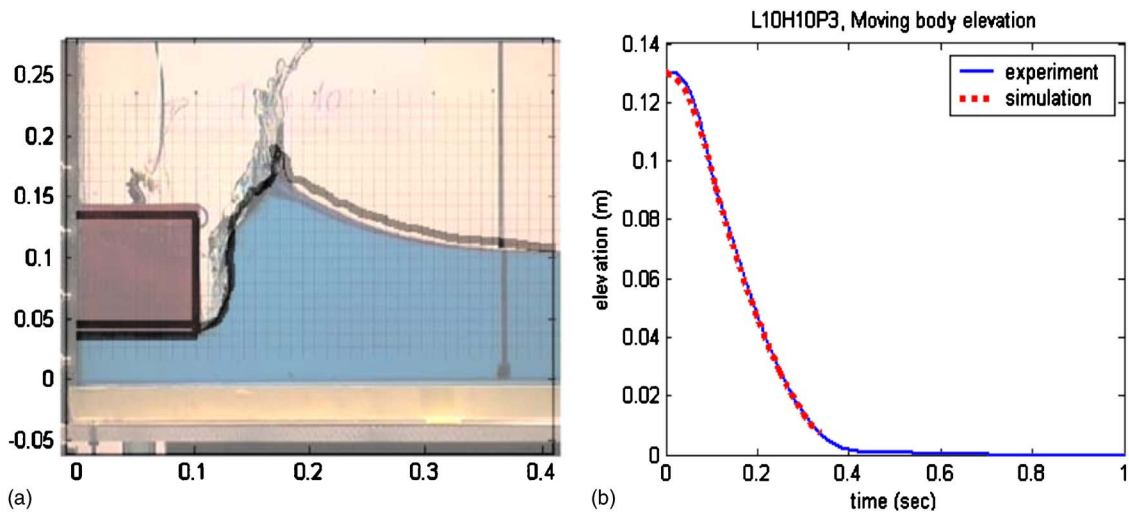


Fig. 6. Snapshot of position of rigid body and free surface profile at $t=0.32$ s (a); displacement time history of moving rigid body (b) (Case II, Test L10H10P3)

413 for Case I. Note that, for the initially submerged bottom drop, 422
 414 turbulence is generated at the bottom surface as the fluid below 423
 415 the falling rigid body is being pushed aside and a vortex is formed 424
 416 (where the turbulence intensity is the highest) at the sharp corner 425
 417 as expected. Based on an examination of the numerical data (not 426
 418 shown here due to space limitation) the turbulence intensity in- 427
 419 creases as the rigid block continues to fall, and as shown in the 428
 420 figure, the vortex becomes detached from the rigid body once its 429
 421 motion stopped. The vortex then attaches to the bottom boundary 430

and propagates downstream with the surface wave created. The 422
 turbulence intensity decreases as the vortex moves further down- 423
 stream due to energy dissipation. 424

In Case II, because of the higher initial elevation and in air 425
 acceleration of the body, the maximum pressure and turbulence 426
 intensity obtained were higher than the initially submerged rigid 427
 body drop test of Case I as anticipated. In fact, as shown in Fig. 428
 14(b), in addition to the turbulence intensity generated at the rigid 429
 body bottom surface, higher turbulence intensity also occurs at 430

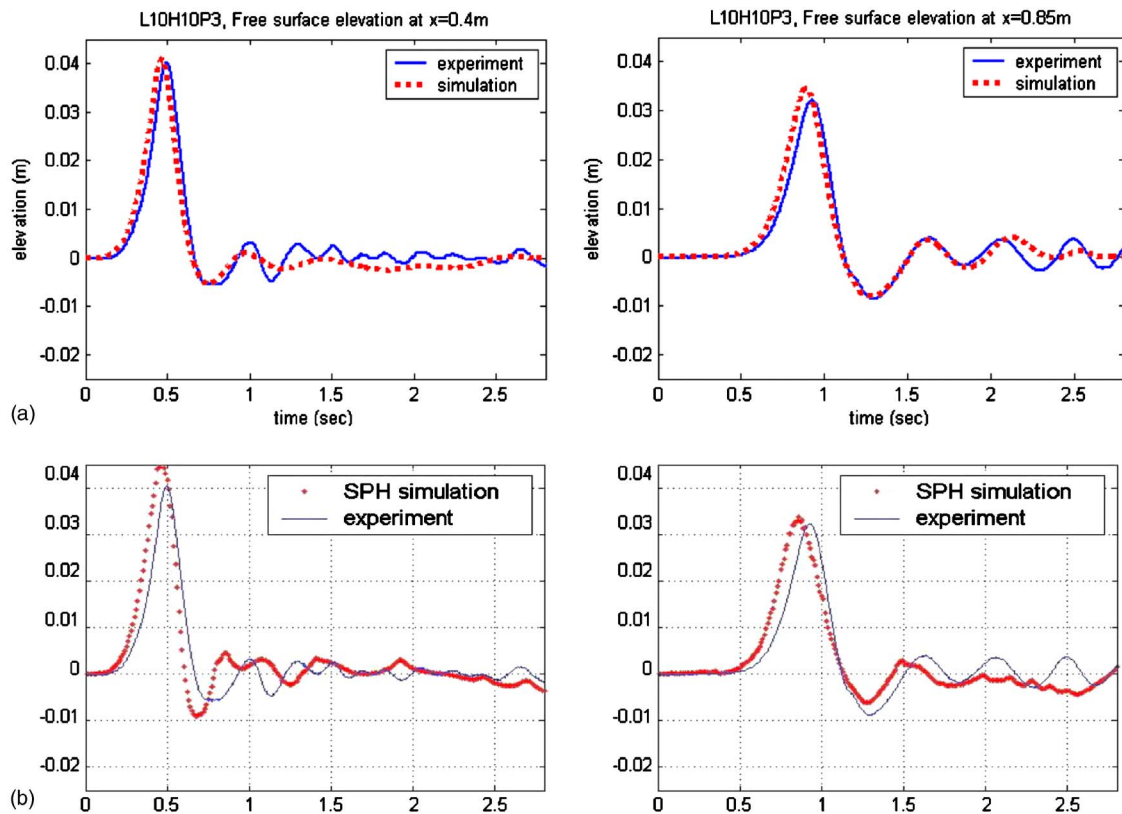


Fig. 7. Experimental data and numerical results [RANS model in (a); SPH model in (b)] for time histories of free surface elevation at $x=0.4$ and 0.85 m (Case II, Test L10H10P3)

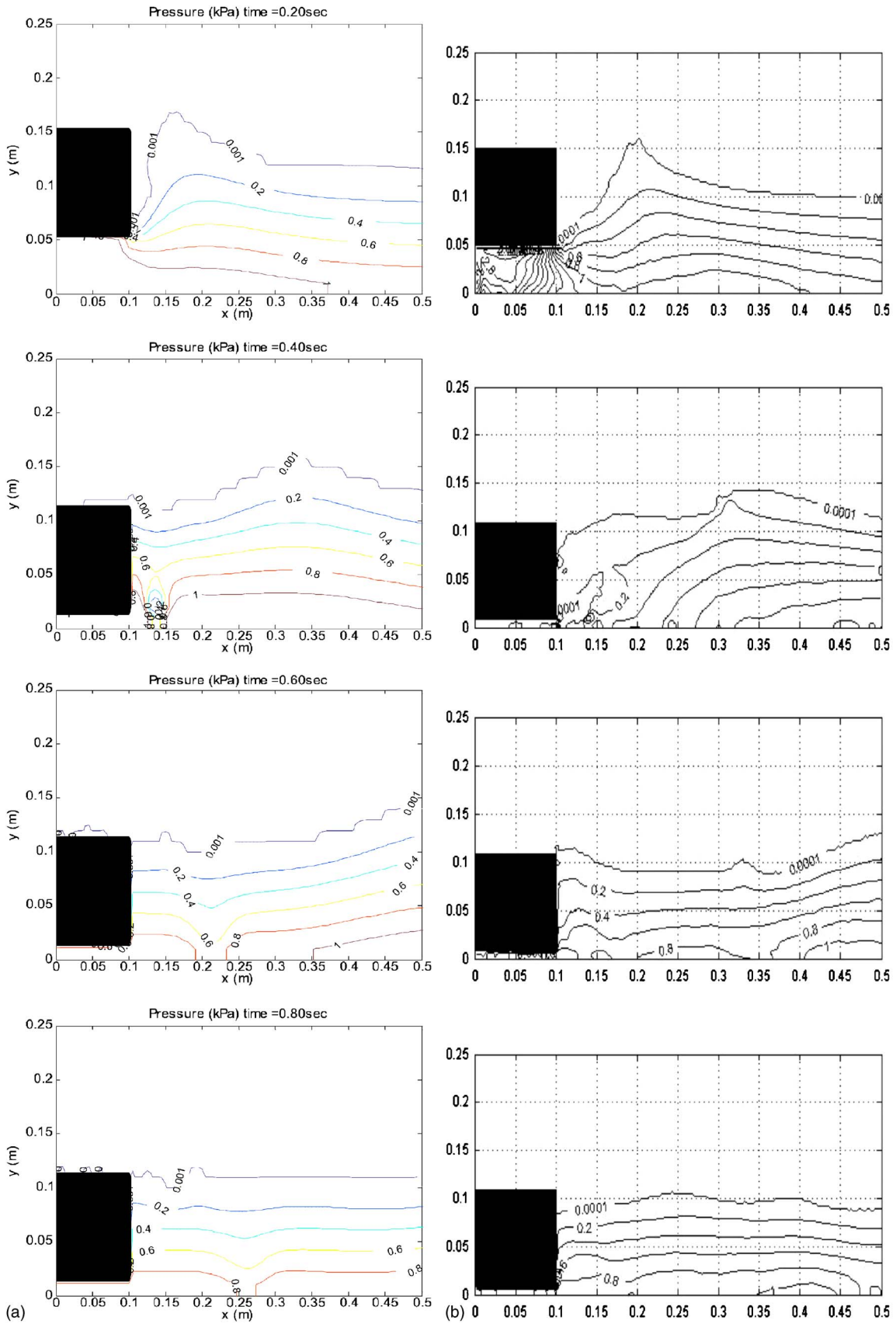


Fig. 8. Contour plot of pressure field computed by RANS (a); SPH (b) at $t=0.2, 0.4, 0.6,$ and 0.8 s (Case II, Test L10H10P3)

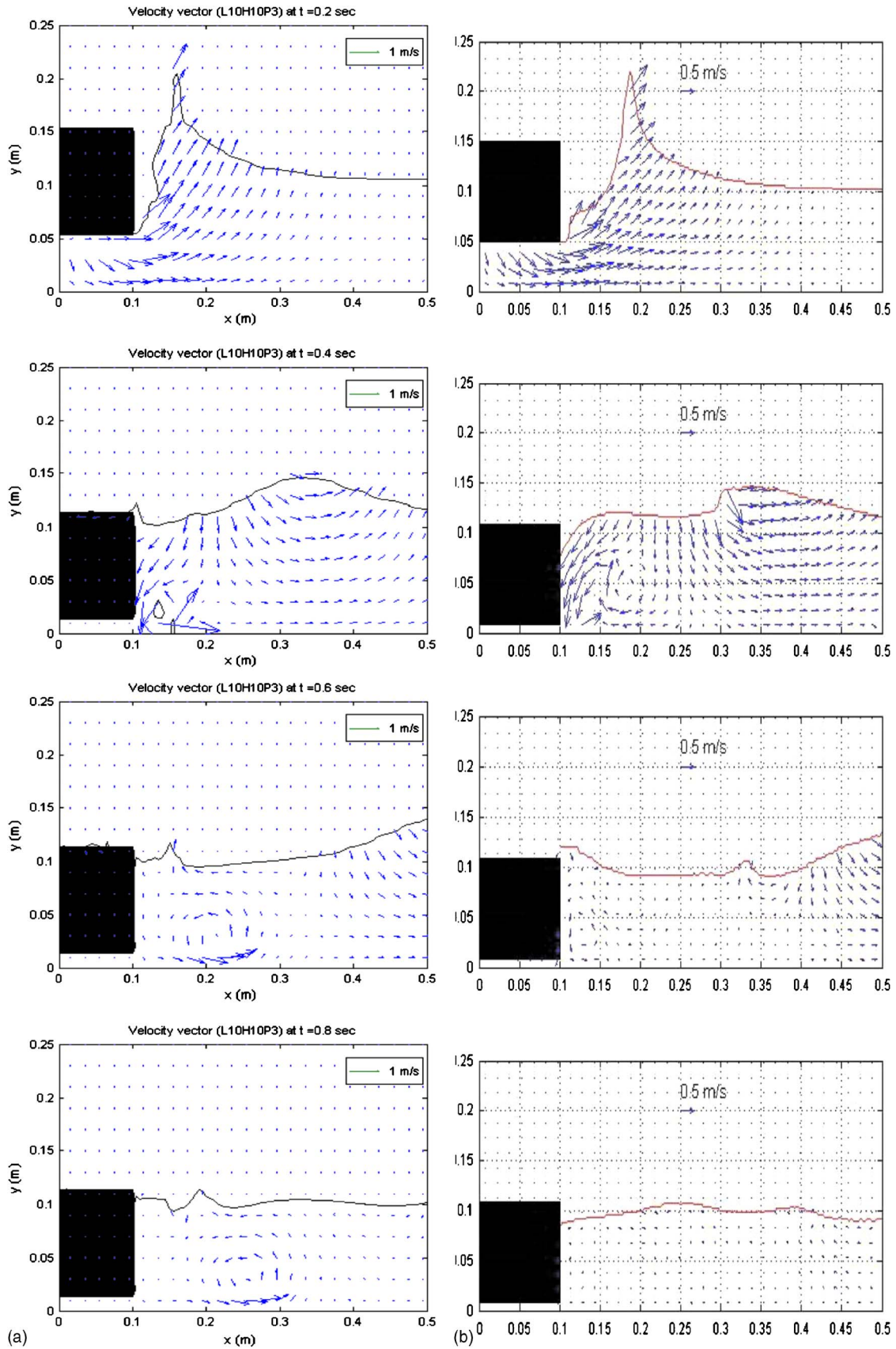


Fig. 9. Vector plot of velocity field computed by RANS (a) model; SPH (b), model at $t=0.2, 0.4, 0.6,$ and 0.8 s (Case II, Test L10H10P3)

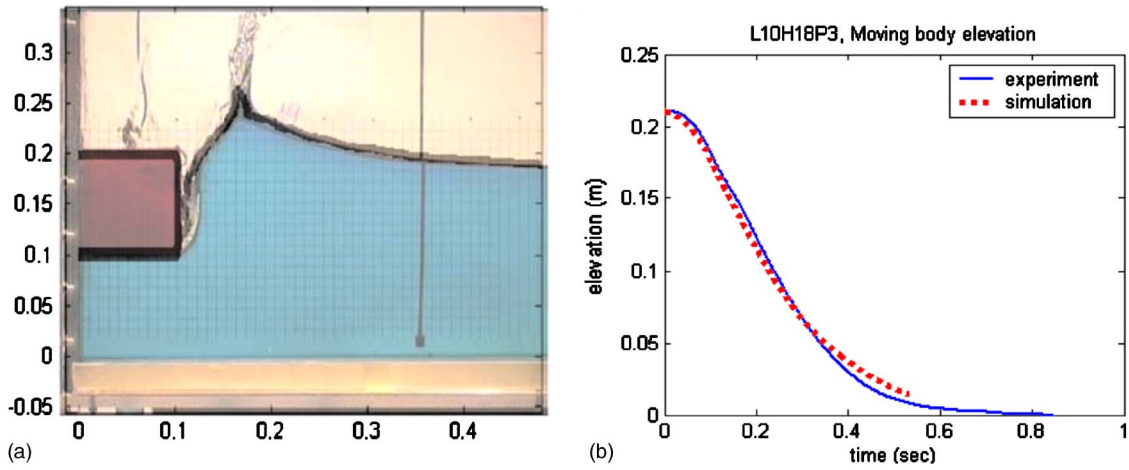


Fig. 10. Snapshot of position of rigid body and free surface profile at $t=0.32$ s (a); displacement time history of moving rigid body (b) (Case III, Test L10H18P3)

431 the free surface of the wave, which is separated from the vertical
 432 body surface on the right hand side. After the falling motion of
 433 the rigid body has ceased, the vortex generated at the sharp corner
 434 propagates downstream as in Case I discussed above. By the time
 435 $t=0.8$ s, the vortex has not traveled as far downstream as that in
 436 Case I and turbulence at the rigid body surface still persists.

437 Fig. 14(c) shows the time evolution of the turbulence intensity
 438 of the fluid in the vicinity of the falling rigid body for Case III. As
 439 expected, the initial fluid flow and turbulence behavior for this
 440 case are identical to that of Case II because of identical body and
 441 initial elevation with respect to the SWL [see top diagrams of
 442 Figs. 14(b and c), $t=0.2$ s], and fluid motion has not yet propa-

443 gated to the bottom of the shallower depth, thus the difference in
 444 bottom boundary conditions (different depths) has no influence on
 445 the flow. The flow and turbulence behaviors of Case III begins to
 446 differ from those of Case II when the influence of the bottom
 447 boundary of Case II becomes noticeable, as shown in $t=0.4$ s in
 448 Figs. 14(b and c). At this time, the motion of the rigid body in
 449 Case II has stopped and the vortex at the sharp corner begins to
 450 propagate downstream. However, for Case III, the rigid body is
 451 still falling and the fluid originally displaced by the falling body
 452 returned over the top of the body with high turbulence intensity.
 453 As the rigid body continues to fall to a large depth, the vortex

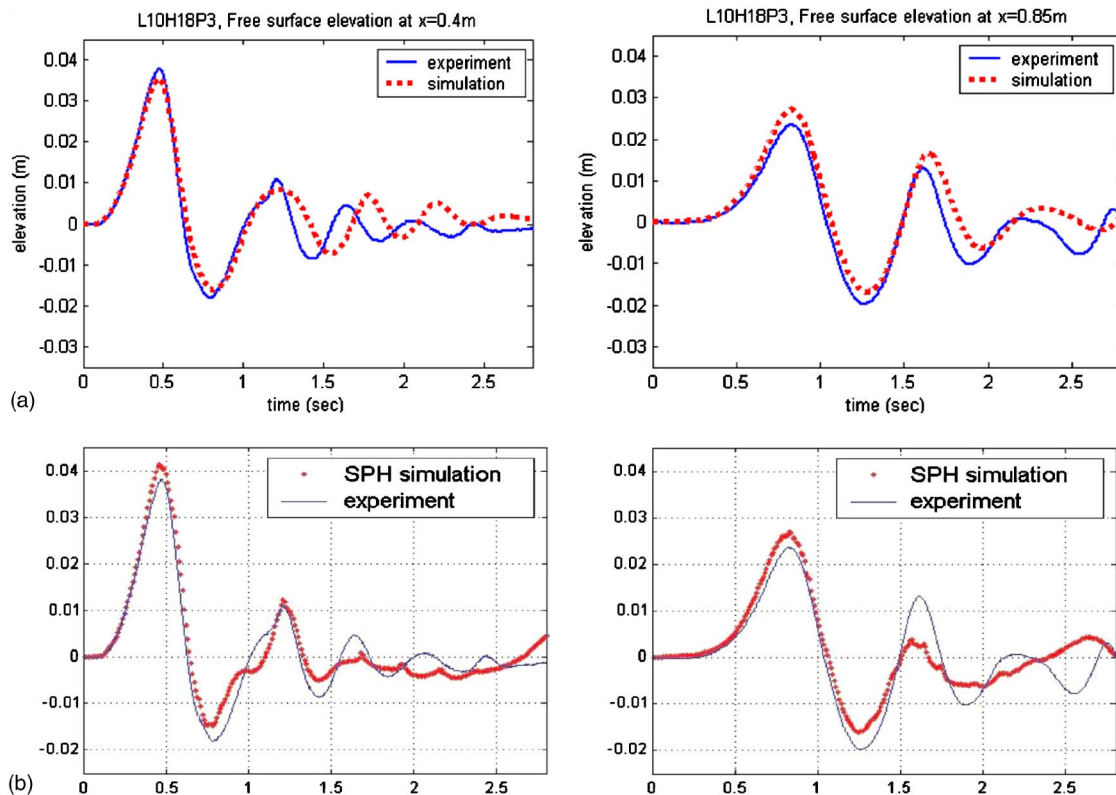


Fig. 11. Contour plot of pressure field computed by RANS model (a); SPH model (b) at $t=0.2, 0.4, 0.6,$ and 0.8 s (Case III, Test L10H18P3)

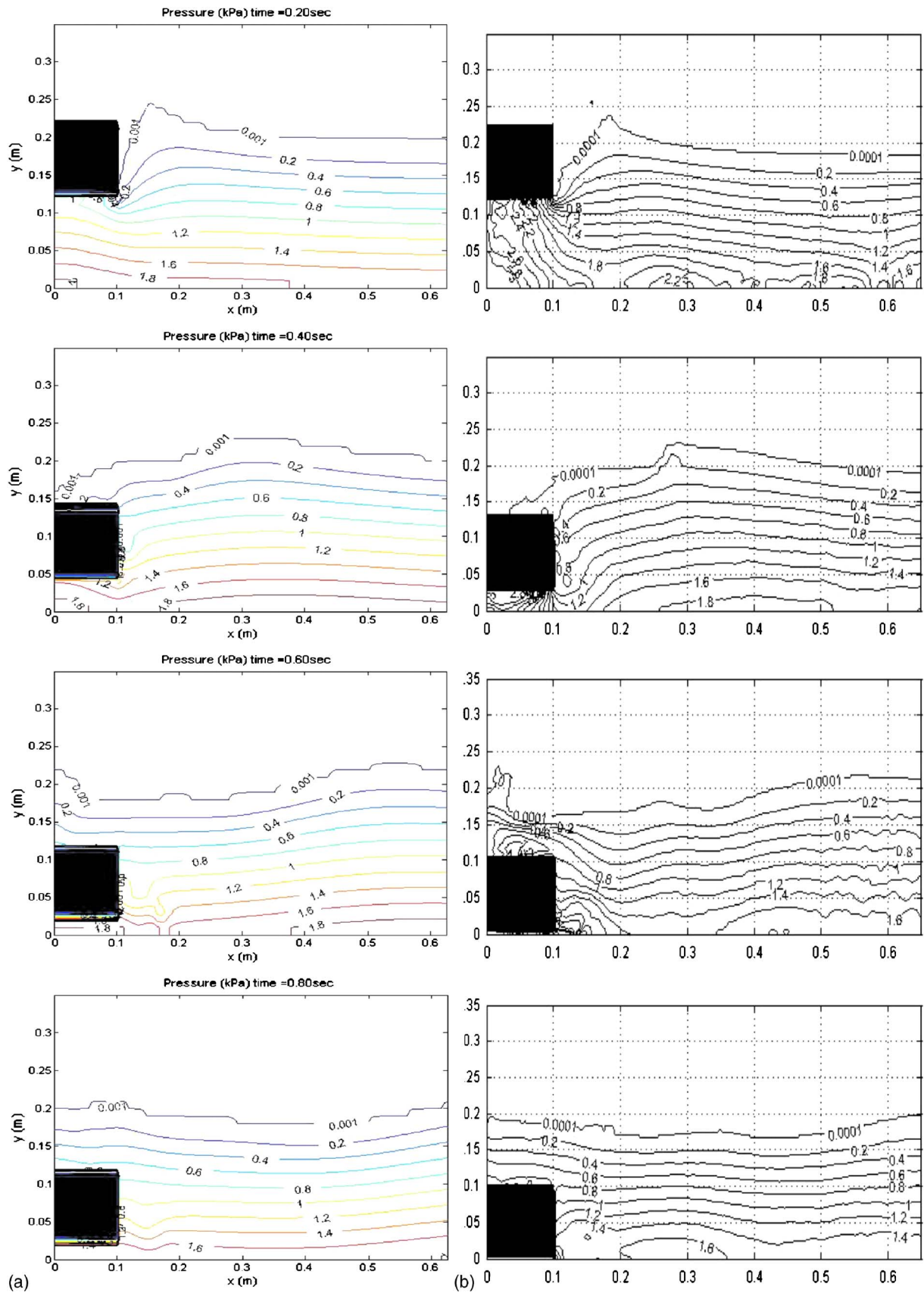


Fig. 12. Vector plot of velocity field computed by RANS model (a); SPH model (b) at $t=0.2, 0.4, 0.6,$ and 0.8 s (Case III, Test L10H18P3)

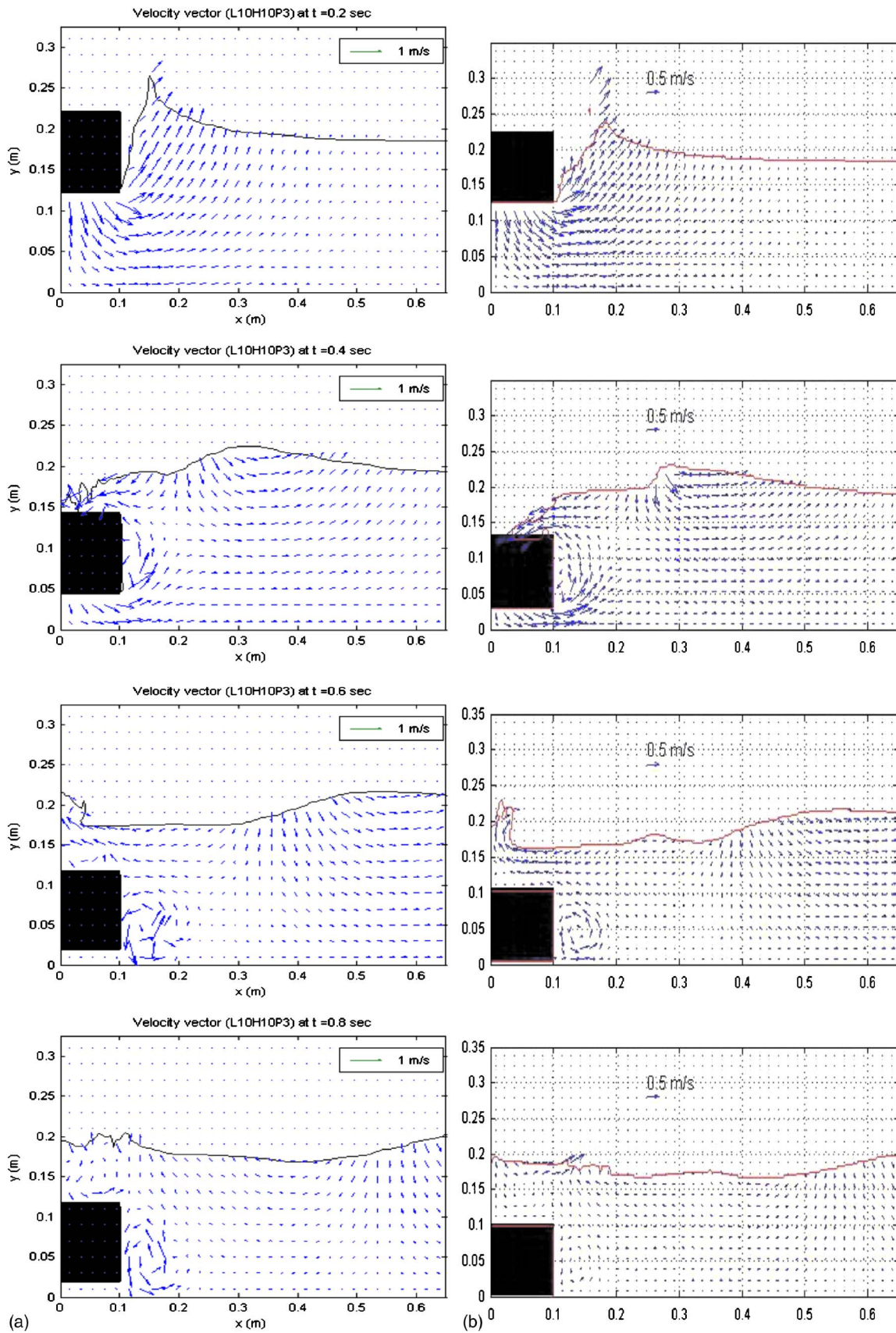


Fig. 13. Experimental data and numerical results [RANS model in (a); SPH model in (b)] for time histories of free surface elevation at $x=0.4$ and 0.85 m (Case III, Test L10H18P3)

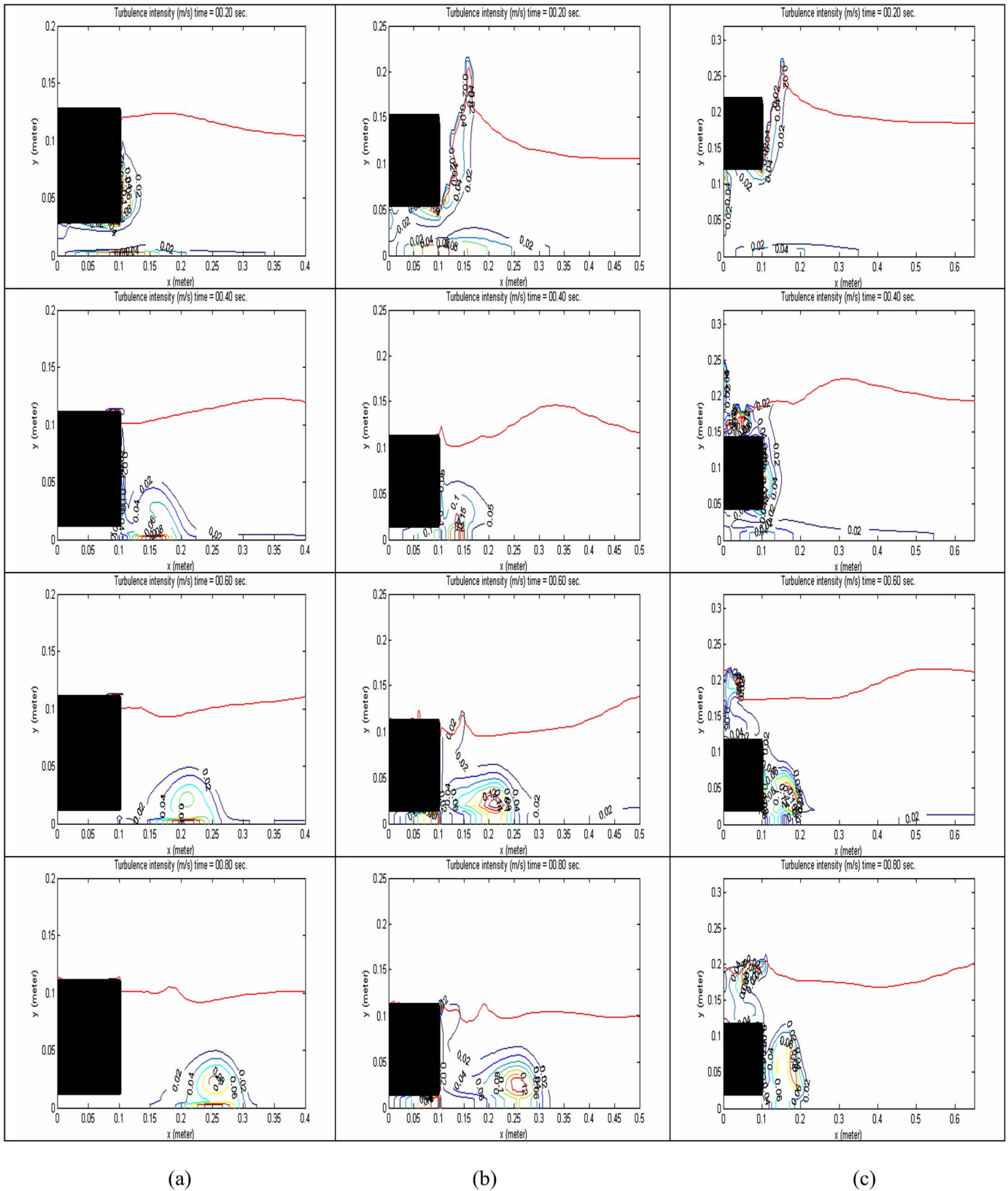


Fig. 14. Turbulence intensity (m/s) computed by the RANS model at $t=0.2, 0.4, 0.6,$ and 0.8 seconds: (a) Case I, Test L10H10M3; (b) Case II, Test L10H10P3; and Case III, Test L10H18P3 (note the vertical and horizontal scales are different for the three cases)

454 generated at the sharp edge continues to intensify and thus has the
 455 highest strength among the three cases [see Fig. 14(c) for $t=0.6$
 456 and 0.8 s].
 457 Note that energy dissipation can be observed in all three cases
 458 when the body motion has ceased and the vortex leaves the edge
 459 and begins to propagate downstream. We want to point out that a
 460 validation of the turbulence intensity model capability cannot be
 461 provided in this study because of the lack of experimental veloc-
 462 ity field data. It is recommended that a velocity measurement
 463 device capable of capturing the details of the velocity fields be
 464 employed in a future study so that the accuracy and validity of
 465 numerical results can be examined more thoroughly.

466 **Relative Magnitude of Shear and Pressure Forces on** 467 **Rigid Body**

468 Finally, to determine the validity of the assumption that the shear
 469 forces on the rigid body surfaces are negligible, the ratio between
 470 the shear stress and the corresponding normal stress on the top,
 471 front, and bottom surfaces of the rigid body are computed from
 472 the RANS model for the three test cases at several time intervals.
 473 As a typical example, for Case III (Test L10H18P3) at $t=0.4$ s,
 474 we found that the shear to normal force ratios on the top, front,
 475 and bottom surfaces of the moving rigid body are (0.057N/
 476 26.578N) 0.21%, (0.554N/78.567N) 0.71%, and (0.393N/
 477 155.960N) 0.25%, respectively. We noted that in general, the ratio
 478 of shear to normal force at each face is less than 1% throughout
 479 the simulation period, thus validating the assumption. Because
 480 there is no experimental measurement of pressure and forces
 481 available to determine the accuracy of the numerical predictions,
 482 it is not fruitful to compare RANS and SPH numerical pressure
 483 and shear force predictions against each other.

484 **Concluding Remarks**

485 Two 2D numerical models—the RANS with a VOF free-surface
 486 capturing method and the SPH—have been presented. The capa-
 487 bility and accuracy of these models are validated by comparing
 488 numerical results with experimental data involving wave genera-
 489 tion by dropping a rigid body at various heights into a 2D flume
 490 partially filled with water (Scott Russell wave generator). In gen-
 491 eral, the numerical results from both models are in good agree-
 492 ment with experimental data in terms of the displacement time
 493 history of the falling cylinder and the free surface elevation time
 494 series. The RANS model appears to be able to better predict the
 495 amplitude and phase of the trailing waves than the SPH model.
 496 The SPH model consistently predicts higher dissipation of these
 497 waves at given fixed locations.
 498 The differences in the velocity field between the two models
 499 are significant. This could be the result of different numerical
 500 resolution employed in these models. We recommend that more
 501 detailed experimental measurements of the velocity field be col-
 502 lected in a future study to further validate the numerical models.

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 frane in corpi idrici: meccanica della generazione e della propa-
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